

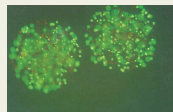
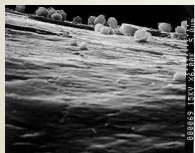
# SIZE DISTRIBUTION ?

Denis poncelet

## Size ?

- ⊙ Diameter = first property of the capsules
  - ⊙ Define largely
    - the membrane or coating surface, then quantity
    - the mechanical resistance
    - the fluidisation and flowing properties
    - the active loading and quantity
- ⊙ Needed for most modelling of
  - the membrane formation
  - the release profile
  - the biocatalyst kinetics (mass transfer)

## Size ?



From a few micrometers ... to a few millimeters

## Size distribution ?

- ⊙ Mono-dispersion ?
  - do not believe pictures
- ⊙ Narrow size distribution allows
  - better microcapsule formation control
  - easier modelling
  - more homogeneous properties
- ⊙ Narrow size distribution
  - = higher cost & lower production

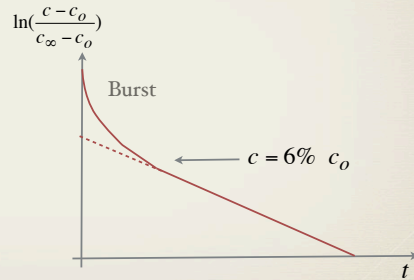
# Size distribution ?

Controlled release



$$\frac{dc}{dt} = -D \frac{(c - c')}{e}$$

$$\ln\left(\frac{c - c_0}{c_\infty - c_0}\right) = -k t$$



Burst effect ? ... no size distribution

# Size distribution ?

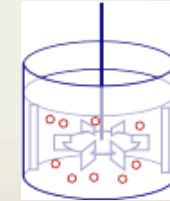
Mechanical resistance



$$v_{breakage} \div d^4$$

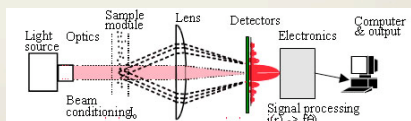
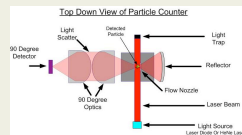
$$d = 500 \text{ to } 1000 \mu\text{m}$$

$v_{breakage}$  varies from 1 to 16



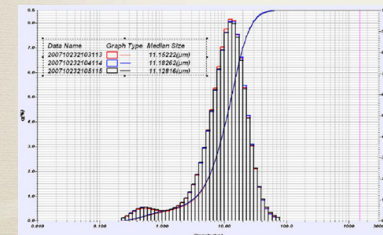
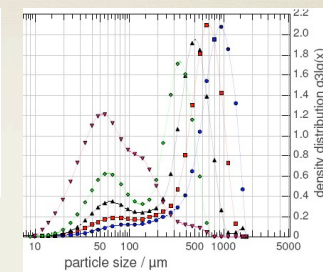
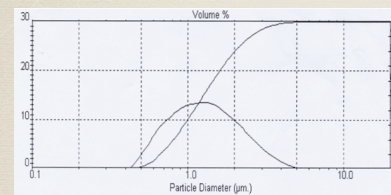
# How to measure the size ?

- Sieving analysis
- Microscopy
- Counting
- Laser diffraction
- Acoustic spectroscopy



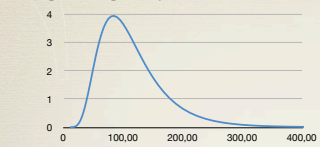
[http://en.wikipedia.org/wiki/Particle\\_size\\_distribution](http://en.wikipedia.org/wiki/Particle_size_distribution)

# Size distribution



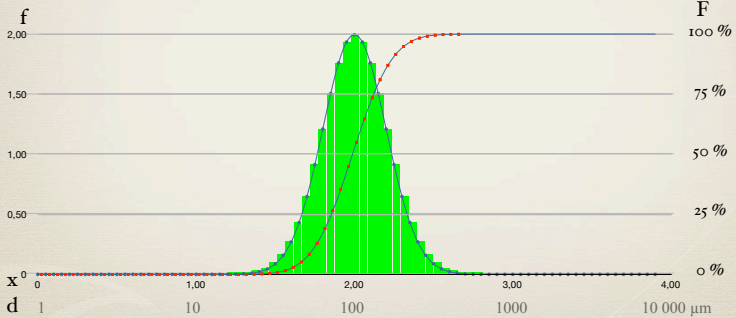
# Histograms

% of particles per 20 μm



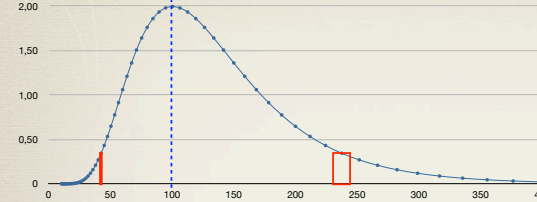
$$f = \frac{dF}{dx} = \frac{1}{\sigma \sqrt{2\pi}} \exp \left[ -\frac{(x-\bar{x})^2}{2\sigma^2} \right] \quad x = \log(d)$$

$$F_x = \int_0^x f dx \quad \text{or} \quad \sum_0^x f \Delta x$$

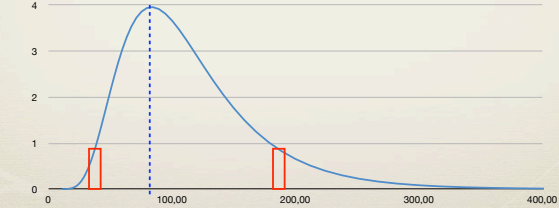


# Histograms

% of particles per class



% of particles per 20 μm

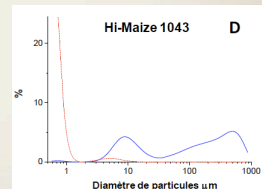
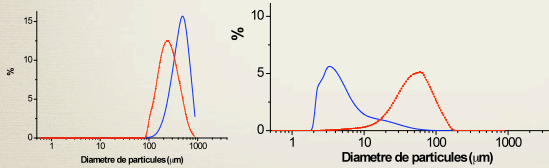


# Frequency !

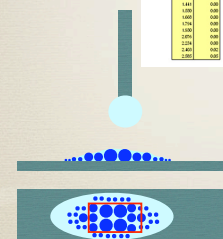
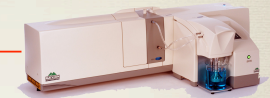
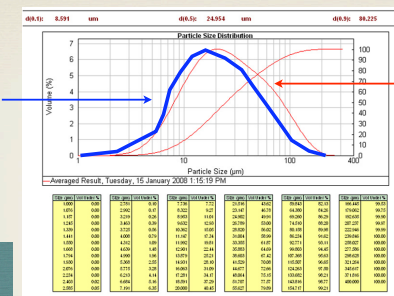
## Frequency

- Numeric,  $f_n$  (microscope)
- Volumic,  $f_v$  (Malvern)
- Massic,  $f_m$  (sieving)
- ...

$$f_s = k x^3 f_n$$

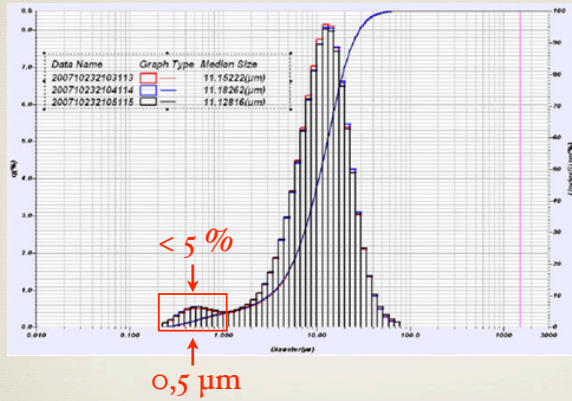


# Fv versus Fn



- Sampling is the key point
- Use raw data, avoid conversion
- Make tendencies not absolute values

# Artefacts



Most probably defaults assimilated to particles

# Mean size ?

- Median = diameter of 50 % cumulative frequency =  $d_{50\%}$
- Mode = diameter of maximum frequency
- Mean size ?

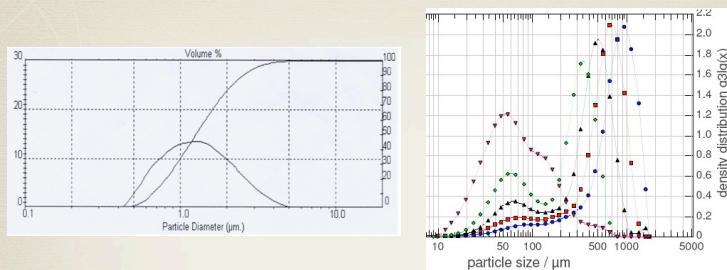
- numeric (microscope)  $d_n = d_{10} = \frac{\sum n_i d_i}{\sum n_i} = f_n d_i$

- volume (Malvern)  $d_{43} = \frac{\sum n_i d_i^4}{\sum n_i d_i^3} = \frac{\sum v_i d_i}{\sum v_i} = f_v d_i$

$$d_v = d_{30} = \sqrt[3]{\frac{\sum n_i d_i^3}{\sum n_i}}$$

- surface  $d_s = d_{32} = \frac{\sum n_i d_i^3}{\sum n_i d_i^2} = \frac{\sum s_i d_i}{\sum s_i} = f_s d_i = \frac{1}{a_s}$

# Mean size ?

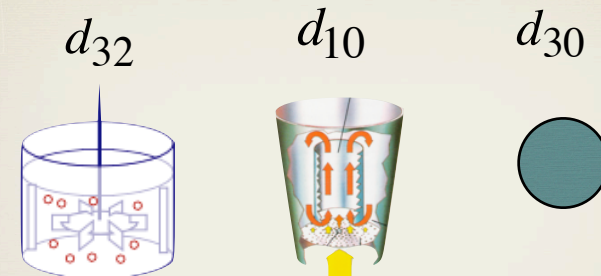


Mean size could be computed for all distributions

Multi-peaks ? multi-means ?

# Which mean ?

- Function of the applications / model



Emulsification  
Mass transfer

Fluidisation

Loading  
Yield

Sometime, mix of mean diameters

# Size dispersion ?

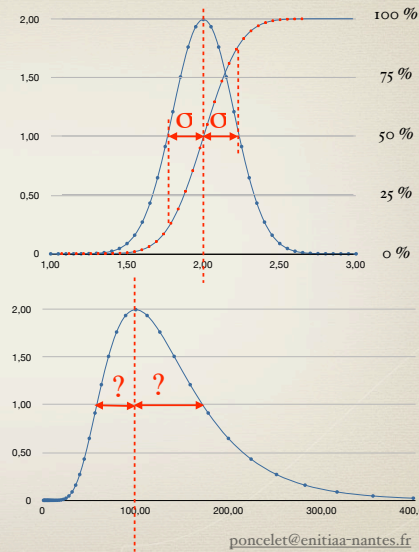
● standard deviation,  $\sigma$

- graphically (!)
- $\sigma = (d_{64\%} - d_{16\%})/2$  (!)

$$\sigma^2 = \frac{\sum f_i (x_i - \bar{x})^2}{\sum f_i}$$

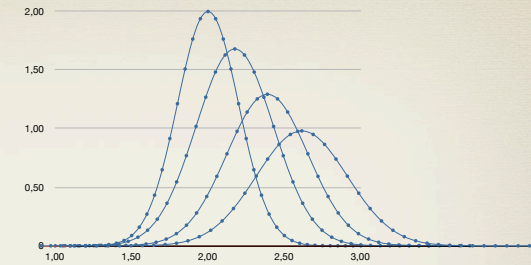
● Distribution

- numeric or volumic
- normal or log-normal

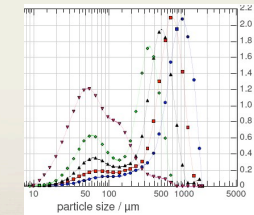


# Standard deviation ?

●  $\sigma' = \sigma / d_{50\%}$



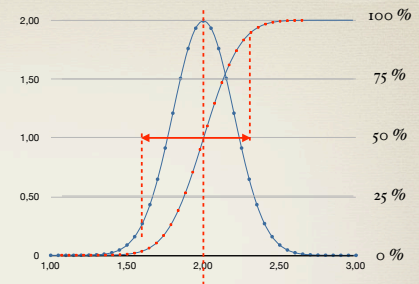
● multi-peaks ?



# Span ?

● Span =  $(d_{90\%} - d_{10\%}) / d_{50\%}$

- relative dispersion
- could be applied to all distributions
- take into consideration most particles
- deviations often under  $d_{10\%}$  and over  $d_{90\%}$



# Conclusions

- Even (apparently) simple measurement needs standard
- Use simplest tool to measure the size
- Beware of the sampling
- Define your mean value
  - mode or median are easier
  - avoid conversion between distribution
- Use span to define dispersion
- Size distribution are not absolute value